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# **Innisfree Village**

# **Alternative On-site Sewage System ENGINEERING REPORT**

14 August 2024



This Alternative Onsite Sewage System (AOSS) design is submitted under the provisions of Section 32.1-163.6 of the Virginia Administrative Code and to the engineer's knowledge, complies with the requirements therein.



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# **OVERVIEW**

The purpose of this document is to present the design criteria and design information for wastewater treatment and disposal for the alternative onsite sewage system (AOSS) to manage sewage for Innisfree Village (Innisfree). Innisfree is a residential community for adults with mental disabilities located in western Albemarle County, north of Crozet, VA. Sewage from buildings at Innisfree Village (Innisfree) is currently managed using conventional onsite sewage systems (COSS) consisting of septic tanks with gravity drainfields.

The Project Purposes are summarized below:

- Replace most of the existing COSS's with a centralized wastewater collection treatment and disposal system permitted as an Alternative Onsite Sewage System (AOSS) through the Virginia Department of Health (VDH). This will provide reliable long-term management of the sewage from the residences and other important buildings.
- Disperse highly treated effluent in a drainfield that is downgradient from the cluster of gardens and drinking water wells in the upper Village area.
- Remove trace organic compounds and nitrogen from the effluent before discharge to the soils to protect the groundwater resources.



## **Table 1. Project Information and Projected Wastewater Flow**

# **Engineering Project History**

An evaluation of the overall water and sewer systems was performed by Inboden Environmental Services, Inc. (IES) in 2021. The conclusion of this evaluation was that a centralized sewer system should be installed to replace the COSS serving most buildings. IES prepared a Preliminary Engineering Report (PER) and submitted a draft version to Ryder Bunce of VDH in Sep. 2022. IES engineering staff had a Preliminary Engineering Conference with Mr. Bunce and Josh Kirtley of VDH. A final version of the PER was submitted in Dec. 2022.

Aqua Nova Engineering took over the project in December 2023. Representatives from VDH, including Mr. Bunce, Mr. Kitley and Steve Thomas reviewed the soils in the proposed dispersal area in February 2024. Subsequently, Aqua Nova performed further soils evaluations to define the variation in soil characteristics and hydraulic conductivity within the area proposed for the primary dispersal field.

# **DESIGN CRITERIA**

# **Wastewater Sources, Flows and Characteristics**

There are twenty-one separate buildings that will be connected to the AOSS. Table A-1 (Appendix A) lists the buildings, information about occupancy and estimated wastewater flows for each building. Also, the existing COSS that serves each building is listed in Table A-1. A summary of design wastewater generation rates by source is presented in Table 2.





(a) Maximum occupancy.

(b) Flow estimated in gallons per person per day

(c) Workstations used by residents and resident staff, up to 3 shifts/day of 7-person teams. Ea. Shift is 2-hours.

(d) Office and one of the workshops are in a single building but usage is estimated separately.

(e) Normal occupancy is four persons for the day shift. Occasionally up to 15 people attend a short meeting.

(f) Proposed future residence with five, 1-person bedrooms.

#### Residential Sewer Flow Estimate

Sewage flows for residences are based on measured water use for three buildings over a period of 11 months. The buildings were chosen to represent a range of usage types and locations. Amity is a larger building in the center of Innisfree and is has extra day use. Meadow is a medium sized residence on the edge of the core area. Trillium is a smaller residence located the at distant, uphill end of the Village; it is the northwest most residence.

A summary of residence measured water use is presented Table 3. The complete water use data is presented in Tables A-6, A-7, and A-8 of Appendix A. Note that the AOSS has seven-day flow equalization, so daily flow variation will be averaged over a week. Because of this, Aqua Nova allowed Innisfree to monitor water usage weekly after some daily usage had been recorded.

<b>Building Information</b>		Average Daily Use		Maximum	
		Per building,	Per Person,	Daily Use	
Name	Residents (b)	gpd	gpd/pers.	gpd/person (c)	Note
Amity	8	255.9	33.9	55.8(d)	$(c)$ $(d)$
Meadow	8	221.0	27.8	43.1	(c)
Trillium	6	110.1	22.5	49.9	(c)
Combined Average (e)		195.6	28.1	49.6	

**Table 3. Water Usage - Residential Buildings with Flow Meters (a)** 

(a) Water use measured with dedicated water meter from 28 July 2023 to 05 July 2024.

(b) Typical number of residents. Actual occupancy is used to compute per person water usage.

(c) Maximum daily per person water usage observed in period.

(d) Amity maximum value likely due to timing of meter readings; the two day average was 39.5 gpd.

(e) Average value for the residences listed.

Water use for the three monitored residential buildings had a combined average of 28.1 gpd per person. To be conservative, Aqua Nova chose a design flow rate of 50 gpd per person for the AOSS design. This is about 1.8 times the combined average personal use. Because sewage flow from all buildings will be combined in the AOSS Primary & Flow Eq. Tanks, the combined numbers are appropriate for the AOSS design. The chosen per capita design flow of 50 gpd also corresponds to the combined average of the maximum daily water usage.

#### Design Wastewater Characteristics

The wastewater is predominantly residential sewage. A smaller amount is generated by office and workshops. The Community Center is used for resident and staff lunches only 5 days per week with an occasional small event on the other days. Aqua Nova used the type of occupancy/usage to estimate loading rates for BOD, TKN and other parameters. Overall design parameters for the new AOSS are summarized in Table 4 with detailed calculations presented in Tables A-3 and A-4 in Appendix A

Detailed flow and loading calculations are presented in Appendix A, Tables A-2 through A-4, and accompanying notes. Note that Aqua Nova used a safety factor in developing the design influent load for BOD and TKN listed in Table 2 so these values are higher than would be computed from values listed in Attachment A and Table 2.



#### **Table 4. AOSS System – Final Design Influent and Effluent Parameters**

(a) Design parameters for sewage flow INTO the septic tanks. See Tables A-2 & A-3, Appendix A.

(b) Computed effluent from septic tanks with effluent filters. See Table A-4, Appendix A.

(c) Values used for design of Treatment and Disposal System. Flow Eq. reduces load from primary effluent.

(d) Design effluent to disposal system based on TL-3 effluent and required nitrogen removal.

(e) BOD5 = Carbonaceous 5-day Biochemical Oxygen Demand. TKN = Total Kjeldahl Nitrogen (organic N plus ammonia). TKN and Total nitrogen are concentrations and loadings are as N.

(f) Alkalinity based on estimated source water measurement plus typical addition due to human use, Table 4-15, Crites and Tchobanoglous, (1998). Alkalinity addition may be required for complete nitrification.

# **ONSITE SEWAGE SYSTEM OVERVIEW**

The sewage system will collect wastewater from Innisfree buildings, treat it, and disperse large effluent in a low-pressure dosed drainfield. This Alternative Onsite Sewage System (AOSS) has three main components, (1) collection (2) treatment (3) dispersal that are described in this section. Because all building sewage flows to existing, functional septic tanks, the effluent from existing septic tanks is collected rather than building sewage. The proposed collection and treatment system layouts are shown in the construction drawing Attachment 1 to this report. High-quality effluent from the treatment system is pumped to a pressure-dosed drainfield system located in an area below the Farm Building and Northeast Barn along the Conservation Easement as shown in the Construction Drawing set and further described in the Dispersal Area subsection.

# **NEW COLLECTION SYSTEM**

Septic tank effluent from regularly occupied buildings will be collected for the new Centralized AOSS using a Septic Tank Effluent Pump (STEP) and Septic Tank Effluent Gravity (STEG) collection system. The following buildings have low use and are not connected due to minimal sewage generation: Violet (garden shed), Cabana, and Pool House; septic effluent from these buildings will continue to flow to their respective existing drainfields.

#### Existing Septic Tanks

Existing septic tanks for the connected buildings will remain in service to provide cost effective primary treatment. All septic tanks will be retrofitted with a septic-tank effluent filter located in an access riser. The existing pipes leading from the existing septic tanks will be intercepted between the septic tank and drainfield and will either flow into pump stations or into a gravity sewer system.

#### STEP/STEG Sewer

The overall collection system collects settled sewage from building septic tanks and is essentially a gravity collection main with sub-mains and laterals connecting to it from buildings or groups of buildings. The sewer system layout and details are shown in the Construction Drawings, Sheets 4 through 9. Table 5 summarizes the applicable regulatory requirements and the design approach to comply with each requirement.

Table C-1 in Appendix C summarizes calculations for the gravity sewer main, including slope, length and flow. Existing gravity laterals are sufficiently sized and will not be changed except to add cleanouts. Due to the low flow rates and general downhill trend from pump stations to the gravity sewer main, STEP transport pipes will 1.5 inch diameter and will be routed as necessary to avoid buildings, roads, and buried utilities as much as possible.

There are four septic tank effluent pump stations. Each pump station will be equipped with two septic effluent pumps and a control panel with an alarm to warn of high water levels or pump faults. One of the pump stations is existing. Pump station calculations are included in Appendix C, Tables C-2 through C-4.

#### Existing D-Boxes and Drainfields

Once the treatment system is completed and ready for commissioning, the pipes from septic tanks to the existing drainfields will be capped after connecting the outlet to the STEP/STEG sewer. Existing distribution boxes (D-Box) and septic drainfields will be left in place. Certain drainfields will be preserved as replacement disposal areas for the new main dispersal area. These drainfields are identified in the Effluent Dispersal Section.

The drainfields in the upper and central part of the Village will not be used again in the future due to potential for contamination of gardens and groundwater. Most other drainfields will also be permanently abandoned due to age, size and location. If the D-Box is found in the process of excavating the new collection system, it be will be removed or filled gravel and the inlets & outlets will be capped.

After the Treatment System and Disposal system are completed and tested, the individual septic tanks will be connected to the main sewer system. After the connection to the main sewer, COSS abandonment applications will be submitted to the VDH with requisite documentation.

<b>Regulation Section</b>	<b>Design Approach and Notes</b>			
9VAC25-790-310. Design factors	The STEP pump stations are equipped with duplex pumps for redundancy and can pump at around 25 GPM. The working volume of the pump stations will store any excess flow.			
	The gravity sewer main sizing calculations are included in Appendix C, Table C- 1. The sizing is based on peak instantaneous flow (including the flow from STEP pumps and one future planned residence) to ensure that the pipe is never more than 70% full. The sewer sizing is all designed to carry over the required minimum design flows for laterals, submains, and mains.			
9VAC25-790-320. Design details	The STEG elements of collection system all will carry settled sewage in 3"-6" pipe which is larger than the minimum required of 1.5" pipe. Gravity sewers will be run in Sch. 40 PVC or SDR-35 PVC pipe with sewer fittings. The specified minimum cover over the gravity sewer pipes is 1 foot which will be sufficient to prevent icing given the insulating properties of PVC and the slugs of pumped wastewater that will be regularly flushing through the main. The calculations in Appendix C, Table C-1 show the flow velocity based on the slope and a Manning's n of 0.011 which is typical for a PVC pipe coated in scum. Larger solids deposits will not occur, because the system received settled and screened sewage.			
9VAC25-790-330. Construction details	We have specified low-pressure air testing for the gravity sewer piping. Detail 9- 2 on Sheet 9 of the plans shows the standard rigid piping backfill detail.			
9VAC25-790-350 Manholes	Cleanouts will be used for the settled sewage gravity collection piping. There are not locations where four or more settled sewage collection pipes intersect. Cleanouts will be located at most every 200 feet and before any junction or bend larger than 30 degrees.			
9VAC25-790-360. Water quality and public health and welfare protection.	New sewer pipes will not be installed in the same trench as water pipe nor installed within 10 feet existing water pipes when running parallel. Details 7-1 and 7-2 on Sheet 7 of the plans show how utility crossings including potable water pipe crossings will be handled.			
9VAC25-790-390. Reliability	Innisfree Village has backup power for residential building and well water systems. This allows building residents to conduct water using activities during a power outage. Any STEP pumps will be connected to the buildings backup power supply to prevent a back-up or overflow of the septic effluent pumping system.			
9VAC25-790-430. Alternatives	All sewage will pass through existing upgraded or new septic tanks with 1/16" effluent filters and into the STEP pump stations which will have duplex pumps, a control panel with float switches and alarm.			
9VAC25-790-440. Force mains	The septic tank effluent pumping systems will discharge into pressure laterals and a forcemain with a diameter of 1.5". The pumping rate is around 25 GPM which equates to a velocity of about 4.5 ft/s. STEP sewer pipes will connect to the gravity collection main with a terminal flushing connection and isolation valves followed by a wye into the gravity main. Pressure testing to 150% of design pressure has been specified. Pipe will be HDPE installed per manufacturer's instructions. Flushing connections will be provided at regular intervals to allow for inspection.			

**Table 5. Sewer Design Summary** 

# **CENTRALIZED TREATMENT**

## **Overview**

The centralized AOSS includes an advanced treatment system. The collected septic effluent will be treated in a multi-step biological treatment process. The high-quality effluent will then be dispersed in a controlled manner to a subsurface dispersal system described in the subsequent section. The centralized treatment system will meet project goals stated in the Overview Section. As stated therein, TOrC reduction is a goal, though not required by Virginia regulations.

The Design Effluent characteristics are listed in shown Table 4. The effluent BOD and TSS will meet Treatment Level 3 (TL-3) as listed in the Virginia Department of Health (VDH) regulations. The treatment will remove more than 50% of the influent nitrogen as part of the requirements for an AOSS. For this project, Innisfree has additional criteria for the treatment system performance and design. Additional project goals include removing a significant amount of TOrCs and dispersing very high-quality effluent to preserve soil absorption capacity.

## **Effluent Total Nitrogen Requirements**

The Innisfree AOSS will meet the requirements of 5 mg/L of total nitrogen (TN) at the project boundary through nitrogen removal in the treatment system and some dilution from rainfall in the Nitrogen Dilution Management Area (NDMA) shown on Sheet 23. Due to the location of the dispersal area and surrounding topography the NDMA is relatively small at about 298,000 sq. ft (6.84 acres) so the treatment system effluent must have relatively low TN to meet the boundary limits. A summary of the inputs and calculations of the effluent Total Nitrogen Dilution Model developed by Aqua Nova Engineering is presented in Table 7. The full calculation summary is in Appendix B, Table B-2 Nitrogen Dilution Calculations.



#### **Table 6. Nitrogen Dilution Model Summary**

(a) Design hydraulic loading capacity of drainfield = Equalized flow times factor of 1.05.

- (b) Design final effluent from treatment system
- (c) Assumed value for relatively steep area with full grass / meadow plant cover.
- (d) Assumed value for relatively steep area with full grass / meadow plant cover.

# **Primary Treatment and Flow Equalization**

At Innisfree, septic tanks connected to the buildings provide initial primary treatment, removing most solids, settleable and floating waste components. The septic tank effluent from all connected buildings will discharge into a primary settling and filter tank located at the main treatment system. This tank has dual effluent filters and will remove any residual solids or oil/grease that may have escaped the building septic tanks. This will minimize trash and other constituents that could negatively impact the rest of the treatment process.

Effluent from the primary screening process will be overflow into The Flow Equalization tank that is sized to equalize flow over seven days. This attenuates daily peak flows and higher flows from weekdays and or events. Duplex pumps in the Flow Eq. Tank are activated by the control panel in timed doses to deliver a relatively steady flow to the Secondary Treatment system. In the event of very high levels in the Eq. Tank there is a gravity overflow pipe into the Pre-Anoxic Bioreactor tank.

Because sewage flows may be at design levels during power outage events, Innisfree has decided that the treatment and disposal system will be on automatic backup power from a generator. The generator will automatically come on during a power outage to maintain wastewater system operation.

#### **Secondary treatment**

The purpose of secondary treatment is to reduce BOD and TSS to TL-3 levels or below. Also, the secondary treatment system will remove significant nitrogen. For this system, high quality secondary effluent is also necessary for the third stage of treatment (Tertiary Treatment). The secondary treatment process is described below.

Secondary treatment will utilize a biological, fixed-film process with a pre-anoxic denitrification reactor. The aerobic fixed film process is the AdvanTex system by Orenco. This proprietary trickling filter system relies microbial communities attached textile strips to treat the wastewater. The wastewater is pumped into a system of sprayers that distribute it over the textile array. This oxygenates the wastewater and brings the wastewater in contact with the microorganisms that convert the waste compounds to benign products and some microbial biomass.

The proposed design includes two stages of recirculating, trickling biofilters to provide a high level of treatment and ensure complete conversion of ammonia to nitrate (nitrification). Nitrified process water is recirculated to an anoxic reactor located downstream of the Flow Equalization Tank which will provide biological denitrification and reduce the incoming BOD somewhat. The secondary effluent will have low BOD, TSS and nitrogen and will receive further treatment in the Tertiary Treatment system.

The secondary treatment process may also provide reduction in certain trace organic compounds. The AdvanTex process appears to have good removal rates for certain TOrCs based on initial literature review. The AdvanTex treatment stage will be followed by tertiary treatment for polishing and additional removal of TOrCs.

#### Pre-Anoxic Reactor

The Pre-anoxic Reactor receives Eq. Tank effluent and recycled flow from the Stage 2 AdvanTex system for biological nitrogen removal. The Pre-anoxic Reactor tank has nominal a volume of 2,000 gallons and will provides about 2.9 hours residence time for the design flow with a 200% recycle rate. The septic effluent pumped in from the Eq. Tank will be anaerobic and high in BOD. The process water pumped back from the AdvanTex system will have significant amounts of nitrate which is used by bacteria to oxidize some of the incoming BOD. The recycle flow will be aerobic so recirculation rates will be controlled to prevent aerobic conditions in the Pre-anoxic Reactor.

The Controller activates pump P10 in the Stage 2 AdvanTex Recirculation Tank to move nitrified process water through the Control Building, where alkalinity can be added as necessary, to the Pre-anoxic Reactor. A propeller mixer will mix the tank contents without adding further oxygen. The Pre-Anoxic tank overflows to the Stage 1 AdvanTex Recirculation Tank #1.

#### AdvanTex System Design

The AdvanTex system will have two stages each with a recirculation tank and dedicated pumps to dose the textile media. The AdvanTex system was designed in accordance with loading and performance criteria provided by Orenco. The design calculations are presented in Table B-1 in Appendix B., and the system is summarized below.

- 1. Stage 1: AdvanTex System. From the Anoxic Reactor, receives controlled doses from Equalization Tank.
	- a. 6,000-gallon recirculation volume consisting of two 3,000 gal. tanks bottom connected. Recirc. Tank 1 volume is about 1.1 times the Equalized Design flow.
	- b. FIVE AdvanTex AX-100 pods (#1-#5), based on BOD mass loading rate.
	- c. Each pod is dosed by a dedicated pump (P3-P7).
	- d. Drains from the AX-100 pods go to a recirculating splitter valve, RSV1.
	- e. RSV1 directs flow back into the Stage 1 recirc. Tank or forward to the Stage 2 Recirc. tank, depending on the level in the Stage 1 Recirc. Tank.
- 2. Stage 2: AdvanTex receives Stage 1 effluent from RSV1.
	- a. Provides further BOD removal and nitrification.
	- b. 3,000-gallon recirculation tank with duplex pumps (P8 and P9)
	- c. ONE AX-100 pod based on hydraulic loading, dosed by P8 / P9.
	- d. AX-100 pod # 6 drains to RSV2 which either directs flow back into the Stage 2 Recirc Tank or forward to the Stage 3 treatment, depending on the level in the Stage 2 Recirc. Tank.

- 3. AdvanTex ventilation. The AdvanTex units are provided with passive ventilation to provide oxygen to the biofilms in the AX pods. This has been proven effective at supplying sufficient oxygen for BOD removal and nitrification.
- 4. Controls System. the overall system Control Panel will control the AdvanTex dosing pumps. This Control Panel will have user set timing for the AdvanTex dosing to allow operators to adjust dosing timing and rest duration.

## **Alkalinity Addition**

Alkalinity will be added as needed to the recycle pipe to the Pre-Anoxic by a chemical dosing pump (MP2) located in the Control Building and actuated by the Control Panel. The system will include a 50 gal drum for sodium carbonate solution. Operators will need to periodically check pH and alkalinity and adjust the dosing settings to insure adequate alkalinity for complete nitrification.

# **Tertiary Treatment**

A tertiary treatment system will be included in order to provide further and final treatment. This system is designed to:

- Produce very high-quality effluent that maximizes dispersal soils longevity and
- Reduce TOrCs that may contaminate the environment.
- Provide final nitrogen removal to meet design effluent requirements

Aqua Nova selected a dual-media packed bed reactor for TOrC/nitrogen removal that consists of an unsaturated wood chip layer underlain by a saturated rock-sulfur layer. Effluent from the lower layer flows into a moving bed biofilm reactor (MBBR) followed by a settling tank with an effluent filter to capture residual suspended solids.

## Design of the Woodchip + Rock/sulfur Biofilter

This biofilter is surfaced dosed and has three main layers. The top layer is wood chips that will remain unsaturated which favors removal mechanisms for TOrCs. The rock-sulfur layer receives effluent draining through the woodchip layer and provides further denitrification and removal of excess BOD potentially leaching from the woodchip layer. The biofilter details and design criteria are outlined below.

- Lined basin with a media bed area of 320 square feet. This bed area will be covered by a roof structure to prevent rainfall entering the system and minimize plant growth in the woodchip bed.
- Top layer: 24 inches deep. Blend of 85-90% wood chips with 10-15% activated carbon.
	- o The design areal loading rate is 18 gpd/sq. ft. based on research references.
	- o Surface dosed via distribution laterals with holes and flow spreading devices
- Second Layer: 9 inch deep plenum of rain-tank matrix boxes
- Bottom layer of drainage rock with sulfur pellets for anoxic denitrification
	- o Design loading rate is 10 gpd/cu.ft. based on research references
	- o Sulfur provides terminal electron acceptors in the denitrification process

- o Sulfur pellets can be added to the Second layer through pipe ports
- o Collection piping in the bottom layer directs flow out to an effluent/ recirculation basin.

#### Woodchip + Rock/sulfur Treatment Mechanisms

The upper layer will have hardwood chips to support a community of fungal and organisms. The activated carbon in this layer will adsorb TOrCs so that the fungal/microbial matrix can metabolize these compounds. Eventually the wood chips will break down and need to be replaced. This layer can be removed with a sewer vacuum truck and/or careful use of a loader with hand shoveling. The removed material will be composted. The composting process will break down residual TOrCs.

The middle layer is rain-tank matrix boxes installed contiguously to form a 9 inch tall "plenum" zone resting on the bottom rock layer. This plenum zone allows for flow redistribution and a series of dosing ports allows sulfur to be added when necessary to the plenum where it will wash down into the rock layer.

The lower layer will be crushed rock with a nominal 1" size. Elemental Sulfur pellets will be added to the top of this layer during commissioning. The sulfur is slowly oxidized in the process of denitrification so this effluent will have sulfate and potentially sulfides.

#### Final Polishing Reactor

The final polishing moving bed biofilm (MBBR) reactor is designed to remove excess BOD and oxidize sulfides to avoid malodorous effluent. A significant amount of BOD can leach out of the wood chip layer when biofilter is started up and for up to 12 months after. This BOD may not be removed in the anoxic rock/sulfur layer. Also, effluent from rock/sulfur bed may have significant amounts of sulfides. An aerobic MBBR will remove the residual BOD and oxidize any sulfides. The details and design criteria of the MBBR and settling tank are outlined below.

## MBBR

- 2,500 gallon Precast concrete tank with biofilm carriers (media)
- Aeration and mixing provided by a removable, coarse bubble diffuser system
- Air provided by a linear piston air pump supplying 10-12 SCFM.
- The reactor is sized for 100 mg/L of influent BOD with effluent  $\leq$  5mg/L.
- The surface area loading rate for the carriers of 1.4  $g/d$  per m<sup>2</sup> of protected carrier surface area (Reference maximum value is 5 g/d per m<sup>2</sup>).
- Carrier volume will be  $2m<sup>3</sup>$  or about 70ft<sup>3</sup>. This represents about 20% of the reactor water volume to allow good circulation. (Max. recomm. fill is 35% of reactor vol.)

#### Settling Tank

- 1,100 gallon compartment in the Effluent Pump Tank
- Min. residence time of 4 hours at design flow.
- Septic Tank Effluent filter (Polylok PL-625) to prevent solids carryover
- Accumulated sludge will be periodically pumped to the septic tank or hauled off site for disposal.

# **SYSTEM CONTROL PANEL**

The AOSS will be controlled by the central control panel based on programmable logic controllers with a touch screen operator interface. The Control Panel will control all the devices in the treatment system as well as effluent dispersal. The HMI will allow operators to review system status and data and easily change settings for controlled devices. An internet connection to the Control Panel will allow remote access for (1) broadcasting alarms and (2) monitoring and control.

The control panel will be located in the Control Building along with the main electrical panel. Most devices will be powered directly from the Control Panel with built in overload protection. Hand/Off/Auto switches will be provided for critical components to allow for manual operation and testing.

# **CENTRALIZED EFFLUENT DISPERSAL**

The effluent will be pumped from the Effluent Tank to a low pressure-dosed lateral drainfield located about 1,200 ft away to the north northeast. Because of the size of the drainfield and variation in soil qualities in the area, Aqua Nova designed three discrete drainfields each with a low-pressure dosed lateral system. This is described further in the following subsection.

## **General Soils Evaluations**

Aqua Nova engineers (while working at IES) directed HydroGeo Environmental, LLC (HydroGeo) to evaluate soils at Innisfree to identify areas suitable for disposal of the effluent from a centralized treatment system. After extensive initial evaluations in 2022 and 2023, we identified an area of suitable soils at the base of a slope below the "plateau" on which Innisfree is constructed.

On 06 Feb. 2024, representatives of VDH met with Aqua Nova and HydroGeo to review soils evaluations in the main proposed drainfield area. The findings from that review indicated that the soils evaluations in the PER were not entirely correct and the "Percolation Rates" had been overestimated.

After the VDH review, Aqua Nova and HydroGeo prepared additional soil profile descriptions and saturated hydraulic conductivity (Ksat) test to develop design hydraulic application rate for the different soils zones within the proposed drainfield area. The drainfield area has denser soils in the center section with more favorable soils on the side areas. Aqua Nova developed a drainfield design as described below with calculation details in Appendix D.

# **Drainfield Soils Evaluations**

Based on the results of all the drainfield evaluations, Aqua Nova developed a drainfield design of four zones within the proposed drainfield area, identified as Sub-areas or Cells A-D. The Cells and locations of evaluations are presented Figure 1. A summary of soil characteristics and saturated hydraulic conductivity tests (Ksat) results for the drainfield subareas are presented in Table 6. Drainfield Design soils evaluation information is presented in Appendix E, this includes Table E-1 with eh soil profile descriptions and Ksat value summaries. The full field data for the Ksat tests is also included in Appendix E.

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# **Design Hydraulic Application Rates**

Based on the soils evaluations, field observations and Ksat testing results, Aqua Nova developed "Estimated perc rates" and design hydraulic loading rates for the different drainfield sub-areas. The information used to develop these values is summarized below by Sub-Area or Cell. The main soil features, and hydraulic conductivity of the Cells are summarized in Table 7. The "25% GM Ksat" value in Table 7 is derived by dividing the geometric mean of cell Ksat data by 4.





(a) Saturated, clean water, hydraulic conductivity measurements using Johnson Permeameter.

(b) Designated Cell (sub-area) of larger proposed drainfield area. See Figure 1.

(c) Depth of trench bottom below surface.

(d) Most common soil textures for strata at trench bottom (18 inches) and 18 inches below.

(e) Number of separate Ksat tests run for listed depth range.

- (f) Depth from surface to bottom of permeameter.
- (g) Value for developing hydraulic loading rates from VA regs, equal to geometric mean times 0.25.

(h) Geometric mean divided by 10  $(x 0.10)$  converted to gpd/ft<sup>2</sup>.

#### Drainfield Cell (Subarea) A -Design Hydraulic Loading Rate

Drainfield Cell A generally had clay loam soils from 6 to18 inches and for at least 18 inches below that. The exception is SPD 5 located south of the lowest trench closer to the heavier soils in Cell B. The majority of that trench and the rest of Cell A have clay loam soils. The Ksat results range from 12 to 110 cm/d with geometric mean of 44.1. One fourth of the geometric mean is 11 cm/d. This value and the soil textures justify the overall Estimated Percolation rate of 55 MPI with associated hydraulic loading rate of 0.94 gpd/ft<sup>2</sup>. Note that Ksat geometric divided by 10 is equal to 1.08  $\text{gpd/ft}^2$  and the proposed rate is less than that.

## Drainfield Cell (Sub-area) B -Design Hydraulic Loading Rate

Drainfield Cell B generally had clay soils at the trench bottom depth, and for at least 18 inches below the trench bottom depth. About half the SPDs have clay loam soils in that same depth range. The SPDs with clay soils show good structure that will allow decent hydraulic conductivity. The Ksat data results ranged from 5 cm/d to 120 cm/d with geometric mean of 44.1. One fourth of the geometric mean is 6.1 cm/d. The soil structure and Ksat data support the Estimated Percolation Rate of 90 MPI with associated hydraulic loading rate of 0.50 gpd/ft<sup>2</sup>. The geometric mean of Ksat values divided by 10 is equal to 0.60 gpd/ft<sup>2</sup> and the proposed HLR is slightly less than that at  $0.56$  gpd/ft<sup>2</sup>.

#### Drainfield Cell (Sub-area) C -Design Hydraulic Loading Rate

Cell C had a mixture of loam and clay loam from about 6 to 19 inches. For at least 18 inches below the trench bottom depth, the soils were clay loam and clay. The SPDs with clay soils had structure that will allow decent hydraulic conductivity. The four Ksat tests conducted from 28 to 30 inches below grade have a range of 32 to 42 cm/d with a geometric mean of 38 cm/d. One fourth of that is 9.5 cm/d, which along with soil type, support an Estimated Percolation rate of 65 MPI and a design application rate of 0.83 gpd/ft<sup>2</sup>. The geometric mean of Ksat values divided by 10 is equal to 0.94 gpd/ft<sup>2</sup> and the proposed HLR of 0.83 gpd/ft<sup>2</sup> is less than that.

# **Drainfield Design**

Using the geometry of the sub areas, Aqua Nova developed a trench layout for each subarea and calculated the hydraulic capacity of each sub-area. The characteristics and capacity of the subfields in the Primary Dispersal is shown in Table 8. Table D-1 in Appendix D contains more detail on the drainfield design. The overall capacity of the drainfield is somewhat higher than the Equalized Design flow, i.e., design effluent flow.

Note that sub-area D is located uphill of sub-area A. Sub-area D will not be used as part of the Primary Drainfield but will be used for part of the reserve area. Therefore, it is not shown in Table 7.

#### Primary Drainfield System Design Details

The primary drainfield will consist of Sub-areas A, B and C as listed in Table 6. specific details are shown on the construction drawings and are summarized below.

- Low-pressure dosed trenches, three feet wide, using EZ-Flow gravelless modules.
- 11 Zones -flow controlled by solenoid valves and flow balancing valves
- Lateral lengths vary from 75 to 100 ft. Each lateral has a flow balancing valve.

The multiple zones within each drainfield will facilitate effective dosing of the effluent. Low pressure dosing calculations for each drainfield sub-area are presented in Appendix D, including details of each LPD system matched with effluent (P13  $\&$  P14) pump curves

			Dispersal Trench Physical & Design Information				
Cell or Sub-area (a)	Estimated Percolation Rate, MPI (b)	<b>HLR</b> gpd/ft2 (c)	Number of Trenches (d)	Width ft	Length ft	Absorb. Area, ft2 (e)	Hydraulic Capacity gpd(e)
A	60	0.94	9	3	75	2,205	1,904
B	90	0.58	12	3	85	3,060	1,714
$\mathcal{C}$	65	0.83	8	3	100	2,400	1,992
<b>TOTAL</b>						7,485	5,609

**Table 8. Primary Drainfield Design – Characteristics and Capacity** 

(a) Designated sub-area of larger proposed drainfield area as shown in Figure 1 and listed Table 7.

(b) "Percolation Rate" defined in VA regulations, estimated from soil profile descriptions and Ksat results.

(c) Hydraulic loading rate from 12VAC5-610-950, Table 5, based on Percolation Rate and Ksat results for application of TL-3 effluent with LPD loading. See explanation in subsections below

(d) Design number of trenches in dispersal field at 9 ft on center.

(e) Total trench bottom area for absorption of applied effluent.

(f) Total amount of effluent that can be applied to sub-area on a daily basis.

#### Reserve Drainfield Area

Because this AOSS is replacing existing COSS systems and is essentially a repair, a reserve drainfield area is NOT required by VA regulations. However, Aqua Nova believes it is prudent to propose a reserve drainfield system design. The proposed approach uses multiple drainfield areas: Sub-Area D of the new drainfield area and some existing drainfields for specific buildings. The characteristics of the areas to be used for Reserve Drainfield are listed in Table 9. The existing drainfields would need to be retrofitted with pressure dosing to provide the design application rate. The proposed reserve drainfield area specifics are listed in Table D-2 in Appendix D.

Innisfree will be directed to survey the existing drainfields to be used for reserve and create a plan to preserve these areas in perpetuity. This plan will include specific language in the Innisfree planning documents that preserves these areas and access to them.



#### **Table 9. Reserve Drainfield Design – Characteristics and Capacity**

(a) Drainfield Cell D, defined in Fig. 1. is new. Other areas are existing drainfields.

(b) "Percolation Rate" from soils evaluations OR existing COSS permits.

(c) Hydraulic loading rate from percolation rate with TL-3 effluent & LPD dosing (12VAC5-610-950, Table 5.5).

(d) Design number of trenches in dispersal field at 8 ft on-center for Area D and 9 ft on-center for other areas.

(e) Total trench bottom area for absorption of applied effluent.

(f) Total amount of TL-3 effluent that can be applied to sub-area on a daily basis.

#### Groundwater Mounding Analysis

A groundwater mounding evaluation was performed using the spreadsheet model, from Khan et. Al, 1976, provided by VDH. This model was used to evaluate the potential for mounding of effluent underneath the drainfield areas. A separate spreadsheet model was developed for each drainfield Cell (A-C) because each sub-area had different soils and Ksat values. Drainfield cells A-C are aligned along the contours and general slope is perpendicular to the trenches of the three drainfields so the infiltration of adjacent drainfields should not affect each other. Results of this model are included in Appendix D after Table D-1.

The model inputs assumed conservative hydraulic conductivity or permeability values. The vadose zone (K1) permeability was assumed to be only 25% of the median Ksat Value for a given drainfield. The Restrictive Layer permeability  $(K2)$  was set at 25% of K1. The notes section of each mounding model explains that model input values in detail. Even with these very low permeability values, the model predicts no mounding at the design application rates.

# **Low Pressure Dosing System Details**

Effluent from the final settling and filtration tank will flow into a 1,100-gallon nominal volume effluent pump tank. Duplex effluent pumps will pump effluent to the LPD drainfields via an approximately 1,500 ft long transfer pipe. This transfer pipe passes through two flow meters, one located near the treatment system and another at the drainfield area to allow for monitoring of flow, leak detection, and drainfield balancing. A manifold splits flow between the three drainfield Cells (A-C) with manual valves on each for control and balancing to each Cell. Each drainfield sub area has a dedicated zone valve array with manual balancing valves and zone solenoid valves.

The effluent pumps will be programmed to time-dose the drainfield with each dose cycling through the zone valves one at a time. The flow meters will totalize flow to each drainfield zone to allow the operator to more accurately balance flow to each zone in the long term and detect problems with solenoid valves. The solenoid valves will be controlled and powered via a relay panel located near the drainfield to allow manual operation and troubleshooting.

Detailed information about the pump sizing and LPD system including lateral lengths, orifice size and spacing, and headloss are included in Appendix D as Figures D-1, D-2, and D-3. Details on the LPD system's construction can also be found on Sheet 21 of the plans.

# **Controls System and Remote Access**

The entire wastewater treatment and disposal system operation will be fully automated through the Wastewater Controller which includes a Programmable Logic Controller (PLC) with graphic viewing through a smartphone or personal computer. Based on programmed logic, operator input and multiple sensors, the PLC activates all pumps, actuated valves and blowers. The phone/ computer interface allows easy operator control and input. A secure network connection allows remote monitoring and control of the system for designated operators through the internet. This network connection also allows alarms to be sent to designated operators through email.

## **Hydraulic Controls and Overflows**

Water level sensors (float switch assemblies) located in most tanks or basins in the treatment process sense low, normal and high water levels. Flow meters in the system measure flow into the treatment system and disposal area. Water levels, flow rates and pumps' operational status are monitored by the Wastewater Controller at all times. High water levels will be logged in the Controller and flagged for operator review. Critical high water conditions will trigger an alarm that will be broadcast to designated operations staff.

If water reaches a critical level in the Stage 2 Recirc tank, the Eq. Tank pumps will be disabled and an alarm created. These safeguards prevent spills of untreated wastewater from the wastewater system.

# **REFERENCES**

- 1. Crites, R. and Tchobanoglous, G., 1998. Small and Decentralized Wastewater Management Systems. McGraw- Hill.
- 2. McQuarrie, J. and Boltz, P., 2011. Moving Bed Biofilm Reactor Technology, Process Applications, Design and Performance, Water Environment Research, Vol. 83, No. 6.
- 3. Tchobanoglous, G., and Burton, F., 1991. Wastewater Engineering Treatment Re-use and Disposal, Metcalf and Eddy, 3<sup>rd</sup> Edition, McGraw- Hill.
- 4. Water Environment Federation, 2010. Biofilm Reactors WEF MOP 35. McGraw-Hill.

# **Appendix A**

# **Flow and Loading Calculations**

- **Design Flow and Loading Calculations**
- **Flow Equalization Volume Calculations**
- **Detailed Water Use Data**

Printed: 8/14/2024

#### **Appendix A** - Design Wastewater Flow and Characteristics



#### **Table A-1. EXISTING Buildings, Occupancy and Sewage System Information**



(a) Building number and street address. All are listed as Crozet, VA 22932

(b) Based on VDH permits currently available.

(c) Based on permits from VDH, or where no permit is available, from 2017 "Preliminary Engineering Report" by C. F. Greenberg . Field verify as necessary.

(d) Septic system record is unclear.

(e) Operation Permit was obtained from Health Department

(f) Information is from the septic permit for Community Center (5483 Innisfree Ln.) Need to confirm all information for this well

(g) Workstation Buildings are used by up to 3 shifts of seven-person teams, each there for 2 hours max. Flow is assumed as 1 toilet use + misc.

(h) Office and Workstation Buildings are joined. Office staff is listed separately from worstation staff.

(i) Buildings are not residences and have only occasional use.

**Appendix A** - Design Wastewater Flow and Characteristics



#### **Table A-2. Sewage Flow Estimated from Buildings Connected to AOSS (a)**



(a) Regularly occupied buildings including residences, offices, workshops & Comm. Cntr. NO pool & Cabana

(b) Current Residential Buildings per Table A-1.

(c) Farm building used for egg processing. Day use only; typical use is 3-5 employees with occas. meetings.

(d) Potential future expansion under consideration by Innisfree.

#### **Table A-3. Waste Loading (Raw Sewage) Resulting Concentrations**



(a) Reference value for BOD and TSS daily mass load from VA Regs (Reference 1), Table 5.1. Residents = "Dwelling"

(b) Values for TKN are the typical per capita values for individuals per Wastewater Engineering text. See note (c)

(c) Based on "Quantity of Waste Discharged by individuals on a dry weight basis, Typical without ground up kitchen waste", Metcalf and Eddy (Ref. 2), Table 3-12, p.

(d) Values for TKN are the 1/3 of the per captia values for individuals for 8 hour shift. See note (c)

(e) Short term visit and/or lunch. Values for BOD are 1/5 of per capita values per note (a) andfor TKN are 1/5 values per note C.

#### References

1. Commonwealth of Virginia, Adiministrative Code, 12VAC5-610-670.

2. Tchobanoglous, Burton and Stensel [Metcalf and Eddy], 2002, Wastewater Engineering, fourth ed., McGraw Hill, Inc.

3. Crites and Tchobanoglous, 1998, <u>Small and Decentralized Wastewater Management Systems,</u> McGraw Hill, Inc.

#### **Appendix A** - Design Wastewater Flow and Characteristics

**Project Name: Innisfree Village - Alternative Onsite Sewage System**Updated: **8/8/2024**By: *D. Maciolek* 

#### **Table A-4. Design Criteria -Wastewater Treatment and Disposal (a)**



(a) Flow, loading and resulting concentrations for design of biological treamten system, secondary clarifier and disposal system.

(b) Estimated flow and calculated load after reduction in primary treatment System and resulting concentration.

(c) Equalized flow and load for design of tratment systems..

(e) Estimated percent reduction in Primary Treatment, i.e., septic tanks with effluent filters.

(f) Percent removal based on influent to secondary treatment

Wastewater Treatment System Design Date Printed: 8/14/2024

# **Appendix A** - Flow Equalization Calculations

Project Name: **Innisfree Village - Alternative Onsite Sewage System** *DJM* 8/14/2024 Updated by:

Peak Daily Flow (gpd), from Table A-2. 6,681

#### **Table A-5. Equalization Volume & Average Flow**



(a) Reduction in flow on gived day for reason(s) listed

(b) Flow for day based on peak flow less reductions listed.

(c) Design Discharge to treatment and disposal system

(d) Water volume in Equalization Tank (at midnight) = Start Vol. + Daily Flow - Daily Discharge.

(e) First value is average of all days flow. Second value is DESIGN flow to treatment and dispersal system.

(f) Maximum value of "Volume in Tank".

(g) Working volume above pump minimum submergence and allowing for alarm volume (high water).



#### Table A-6. Detailed Water Meter Data for Amity **Residential Building**



Aqua Nova Engineering, PLC. 434-249-4497 File: Water Meters readings 2023-2024 w\_analysis, Sheet: Amity



#### Table A-6. Detailed Water Meter Data for Amity **Residential Building, contin.**





By: **DJM** 

#### Table A-7. Detailed Water Meter Data for Meadow **Residential Building**



Aqua Nova Engineering, PLC. 434-249-4497 File: Water Meters readings 2023-2024 w\_analysis, Sheet: Meadow



# By: **DJM**

#### Table A-8. Detailed Water Meter Data for Trillium **Residential Building**



Aqua Nova Engineering, PLC. 434-249-4497 File: Water Meters readings 2023-2024 w\_analysis, Sheet: Trillium

![](_page_32_Picture_176.jpeg)

#### Table A-8. Detailed Water Meter Data for Trillium **Residential Building, contin.**

![](_page_32_Picture_177.jpeg)

# **Appendix B**

- **AdvanTex System Design Calculations**
- **Stage Three Treatment Biofilter calculations**
- **Nitrogen Dilution Calculations**

# Appendix B - Wastewater Treatment Design

![](_page_34_Picture_306.jpeg)

# **Table B-1 Orenco AdvanTex® System Design (a)**

![](_page_34_Picture_307.jpeg)

(a) Design of biological treamtment using Orenco Systems AdvanTex® textile trickling filter system.

(b) Each stage consisits of AdvanTex pods and dedicated recirculation tank.

(c) Design Flow and Loading criteria from Tables A-4.

(d) Recommended loading rates from Orenco Systems, Inc. 2017 Design/Engineering Binder.

- (e) Computed required area of Advantex AX unit . Actual area is determined by the number and size of AX units.
- (d) Estimated effluent load based on expected reduction in Stage 1 system.<br>(f) Concentration equivalent computed from effluent load and flow.
- (f) Concentration equivalent computed from effluent load and flow.
- Additional textile plan area provided compared to required computed area = (Provided Area Required Area/Required Area) x %

# Appendix B - Wastewater Treatment Design

![](_page_35_Picture_185.jpeg)

![](_page_35_Picture_186.jpeg)

Ref 1: Evaluation of pilot-scale biochar-amended woodchip bioreactors to remove nitrate, metals, and trace organic contaminants from urban stormwater runoff. Ashoori et. al. 20. Water Research

Volume 154, 1 May 2019, Pages 1-11

#### **Table B-4. - Nitrogen Removal Wetland**

![](_page_35_Picture_187.jpeg)

Ref 2:
Innisfree Village Alternative Onsite Sewage System -Engineering Report

# **Appendix C**

• **Sewer System Design Calculations** 

#### Appendix C - Sewer Collection System Calculations





#### **Table C-1. Septic Tank Effluent Gravity Collection System Calculations -PEAK FLOW (a)**

Manning's "n" Coefficient for PVC coated in sewer scum 0.011



(a) Gravity sewer "Main" that starts where pumped effluent from Trilliium, Halcyon & Oakwood combines with flow from Kenmare and becomes gravity sewer.

(b) Segment start and end points are named for nearest building septic effluent pipe connection. WWTS is the wastewater treatment system.

(c) Negative indicates elevation drop from start to end. Calculated slope is the min. over entire length of segment. Slope to be constant between cleanouts.

(d) Peak instantanous gravity flow rate from septic tanks is assumed to be attenuated by the septic tank.

(e) Residents or users in buildings with sewer connecting to sewer main segment by gravity flow lateral.

(f) Peak instantanous gravity flow rate from septic tanks is assumed to be attenuated by the septic tank.

(g) Pumped flow for this segment is a combination of STEP Pump Station 1 (SPS1) and STEP Pump Station 2 (SPS2) running at the same time.

(h) Maximum community center occupancy. Due to lighter use patterns the GPM instantnous flow per person is reduced.

(i) Maximum office and workshop personnel. Due to lighter use patterns, the GPM instantnous flow per person is reduced.

# Appendix C - Sewer Collection System Calculations









#### Appendix C - Sewer Collection System Calculations





#### **Project Name: Innisfree Village Wastewater System Ugrade** Pumps and Piping **SPS4 Duplex Effluent Pumps to Sewer Main System Curve - Head Loss Calculations** Curve - Head Loss Calculations Updated: 7/31/2024 **Desired Pump Flow** Avg. Avg. **By: CBH Water Velocity in:** Dynamic Losses, ft Total Head gallons per minute Transfer Pump to Transfer Pump to Transfer Product on the Sisch of Transfer Pipe to Disch .<br>ransfe ump Simplex Pump (No<br>Manifold) Velocity, Pipe Pipe<br>Friction Outlet to pipe<br>length Velocity, Minor Minor Paramete Transfer ft/s ft/s Friction Losses Min. lift Max. lift Losses length gpm cfs Pipe length, ft 8 430 0 0.00 0.0 0.0 0.00 0.00 0.00 0.00 **0.0 3.0** Pipe diam., inside (in) <mark>[1.533 ] 1.533 ]</mark> 0.00 0.3 0.01 0.00 0.29 **0.3 3.3** Hazen-Williams Coeff., C 120 120 4 0.01 0.7 0.7 0.05 0.02 0.02 1.03 **1.1 4.1** \* Piping from pump basin to discharge point 6 0.01 1.0 1.0 0.12 0.04 0.03 2.18 **2.4 5.4 Pump Lift \*Additional Head, ft** 8 0.02 1.4 1.4 0.22 0.07 0.06 3.72 **4.1 7.1** SPS1 to SPS2 Min. lift, ft 0 MIN. **0** 10 0.02 1.7 1.7 0.34 0.10 0.09 5.63 **6.2 9.2** PS 1 to Eq. tank Max. lift, ft 3 Max. **0** 12 0.03 2.1 2.1 0.49 0.15 0.14 7.89 **8.7 11.7** 14 0.03 2.4 2.4 0.66 0.20 0.18 10.49 **11.5 14.5** 16 0.04 2.8 2.8 0.86 0.25 0.24 13.43 **14.8 17.8 Minor Losses Number of fittings** 18 0.04 3.1 3.1 1.09 0.31 0.30 16.71 **18.4 21.4** Pump Outlet to Transfer Transfer to Trnsfer\*\* piping Type K discharge 20 0.04 3.5 3.5 1.35 0.38 0.38 20.31 **22.4 25.4** Entrance to manifold 0.5 0 22 0.05 3.8 3.8 1.63 0.45 0.45 24.23 **26.8 29.8** Ball Valve - fully open 0.1 1 24 0.05 4.2 4.2 1.95 0.53 0.54 28.47 **31.5 34.5** Gate Valve - half open 13 0 0 26 0.06 4.5 4.5 2.28 0.61 0.63 33.01 **36.5 39.5**<br>Check Valve 2.5 1 0 28 0.06 4.9 4.9 2.65 0.70 0.74 37.87 42.0 45.0 Check Valve 2.5 1 0 28 0.06 4.9 4.9 2.65 0.70 0.74 37.87 **42.0 45.0** Tee - line flow 0.6 0 30 0.07 5.2 5.2 3.04 0.80 0.84 43.03 **47.7 50.7** Tee - branch flow 1.6 1 32 0.07 5.6 5.6 3.46 0.90 0.96 48.50 **53.8 56.8** 90° Elbow - regular 1.0 3 1.0 34 0.08 5.9 5.9 3.90 1.01 1.08 54.26 **60.3 63.3** 45° Elbow - med. rad 0.25 0 36 0.08 6.3 6.3 4.38 1.12 1.22 60.32 **67.0 70.0** Open pipe disch. | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.08 | 38 | 0.08 | 6.6 | 6.6 | 4.88 | 1.24 | 1.35 | 66.67 | **74.1** | **77.1** Flow Meter - insertion 8 0 **Sum of K values 7.2 2.0 0.0 STEP Tank 2 - SPS2 to STEG** 60 System - Max. Lift System- Min. Lift **X**-Liberty FL50 50 70 O **Total Dynamic Head, ft.** 40 Total Dynamic Head, 30 20 10

0 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24 25 26 27 28 29 30

**Flow Rate, gpm**

#### Appendix C - Sewer Collection System Calculations

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Innisfree Village Alternative Onsite Sewage System -Engineering Report

# **Appendix D**

- **Drainfield Design Calculations- Area and Trench Design**
- **LPD Detail Calculations (Using OSI calculation tool)**
- **Groundwater Mounding Model Results**

# Appendix D - Effluent Dispersal System Design and Configuration



### **Table D-1. Primary Effluent Dispersal Area - LPD Trenches**



(a) Design Percolation Rate developed from soil profile descriptions and Ksat results.

(b) Per Virginia Sewage Handling and Disposal Regulations, 12VAC5-610-950, Table 5.5.

(c) Adsoprtion area is total trench bottom area.

(d) Maximum effluent application capacity equal to Absorption area times Loading Rate (hydraulic loading rate).

(e) Distance between trench centers. Three times trench width for slopes <20% ,Sewage Handling and Disposal

(f) Effective percent of total flow allocated to drainfield area listed. Regulations, 12VAC 5-610, Section 950, F., page 96.

## **Table D-2. Reserve Dispersal Area - LPD Trenches**



(a) Rate for Area D is from soil profile descriptions and Ksat results. Rates for Community Center and Farm Bldg are from existing COSS pern

(b) Application rate Per Virginia Sewage Handling and Disposal Regulations, 12VAC5-610-950, Table 5.5.

(c) Adsoprtion area is total trench bottom area. Adsoprtion Capacity is Adsorption area times Loading Rate (hydraulic loading rate).

(d) Distance between trench centers. Three times trench width for slopes <20% ,Sewage Handling and Disposal Regulations, 12VAC 5-610, Section 950, F., page 96.

(e) "Red Star" Farm building used for egg processing. New drainfield constructed in 2016.

# **Pump Selection for a Pressurized System - Multiple Family Residence Project**

Innisfree Village / LPD dispersal area A

#### **Parameters**



#### **Calculations**



#### **Frictional Head Losses**



#### **Pipe Volumes**



#### **Minimum Pump Requirements**





### **PumpData**

Liberty FL-73M-2 208V, 3 Phase,





# **Pump Selection for a Pressurized System - Multiple Family Residence Project**

Innisfree Village / LPD dispersal area B

#### **Parameters**



#### **Calculations**



#### **Frictional Head Losses**



#### **Pipe Volumes**



#### **Minimum Pump Requirements**





## **PumpData**

Liberty FL-73M-2 208V, 3 Phase,





# **Pump Selection for a Pressurized System - Multiple Family Residence Project**

Innisfree Village / LPD dispersal area C

#### **Parameters**



#### **Calculations**



#### **Frictional Head Losses**



#### **Pipe Volumes**



#### **Minimum Pump Requirements**





# **PumpData** Liberty FL-73M-2 208V, 3 Phase, **Legend**





Innisfree Village Alternative Onsite Sewage System -Engineering Report

# **APPENDIX E**

- **Soils Evaluation SPD and Ksat Summary**
- **Ksat Testing Data sheets**

Project: **Innisfree Village AOSS**  Updated: 8/14/2024 **By:** David Maciolek





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#### **Table E-1. Drainfield Soil Evaluation Summary** т

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#### **Table E-1. Drainfield Soil Evaluation Summary** Т

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# **APPENDIX E**



#### **Table E-1. Drainfield Soil Evaluation Summary** Т

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Aqua Nova Engineering, PLC



(a) Test Pit (pit), soil boring (SB) or Saturated Hydaulic Contductivity Test (Ksat)

(b) Saturated hydaulic contductivity test stabilized rate. Full test data is presented in Appendix E.

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**APPENDIX E**

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